

Glendale Water and Power

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# Phase II Pilot Testing Task 8: Refined Cost Estimates for Hexavalent Chromium Removal Technologies

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A. Technology Cost Estimates



Pilot testing of hexavalent chromium (Cr(VI)) removal technologies revealed that strong base anion exchange (SBA), weak base anion exchange (WBA), and reduction/coagulation/filtration (RCF) could treat contaminated groundwater in Glendale, California to low levels (i.e. less than 5 µg/L, or 95% removal). Using an approach that included the evaluation of vendor cost proposals and standard cost estimation practices, we developed screening-level cost estimates for these Cr(VI) removal technologies in 2005; these initial cost estimates were refined and updated herein to provide feasibilitylevel estimates. Capital costs and operations and maintenance (O&M) costs were estimated to determine the cost drivers for the different technologies. Two different size systems were considered, including 500 gpm wellhead treatment or 1,000 gpm treatment of two wells, as likely technologies for the Phase III demonstration study.

Hexavalent chromium, Cr(VI), is not specifically regulated in drinking water. However, total chromium, Cr(III) plus Cr(VI), has been part of national drinking water regulations The federal regulatory maximum contaminant level (MCL) for total since 1975. chromium is 100  $\mu$ g/L, while the MCL in California is 50  $\mu$ g/L. Although no federal limit has been established for Cr(VI) in drinking water, California's Department of Health Services has a mandate by State law to establish a Cr(VI)-specific MCL. The Cr(VI) carcinogenic *de minimis* risk level established by the State in 1999 was 0.2 µg/L, which contributed to a public health goal (PHG) of 2.5 µg/L for total chromium (OEHHA, 1999). Although this PHG was later rescinded and is currently under review, the potential for a new Cr(VI) MCL and a lower California total chromium MCL motivated the effort to identify treatment technologies able to remove Cr(VI) to levels far lower than the current limits. In addition to identifying such treatment technologies, understanding the treatment costs of these Cr(VI) removal technologies is critically important for regulatory development and drinking water utilities that face chromium treatment in the future.

Significant research efforts spearheaded by the City of Glendale have evaluated treatment technologies for chromium removal at both the bench- and pilot-scale. These efforts were prompted in 2000 by public concern over the presence of Cr(VI) in drinking water. In response to this public concern, the City of Glendale, with the participation of the Cities of Los Angeles, Burbank, and San Fernando, initiated a four-phase program to develop full-scale treatment capable of removing Cr(VI) from San Fernando Valley groundwater, which contains plumes with high concentrations of Cr(VI).

The Glendale four-phase program includes:

- Phase I: A bench-scale study that improved the understanding of fundamental Cr chemistry and screened promising treatment technologies (AwwaRF, 2004),
- Phase II: A pilot-scale study that evaluated treatment technologies for removing Cr(VI) to low levels in Glendale groundwater (McGuire et al., 2006; Qin et al., 2005),
- Phase III: A bridge pilot-scale study and a demonstration-scale study that will finalize the technology evaluation and address additional costs and residuals issues, and
- Phase IV: Full-scale implementation of an effective Cr(VI) treatment technology.

Until this comprehensive program, no treatment technology had been shown to reliably remove Cr(VI) in drinking water to levels below 5  $\mu$ g/L, and no cost estimates of treatment have been developed. This paper reports on the refinement of screening cost estimates for Cr(VI) removal technologies tested in Phase II pilot testing.



Technology cost estimates were refined by: (1) obtaining updated quotes for vendorspecific technology cost information directly from vendors, (2) requesting technology cost information from several vendors for the RCF process, and (3) developing independent cost information using existing literature, professional judgment, and industry cost models. Estimates were developed for two system sizes with design flow rates of 500 gpm and 1,000 gpm.

The American Association of Cost Engineers (AACE) defines five categories of estimates in an effort to establish expected accuracy range for various types of cost estimates. The objective of this work was to refine initial conceptual screening cost estimates to provide study or feasibility-level costs. It is expected that an estimate of this type would a Class 4 estimate accurate within -15% or +30%.

Estimate Class	Level of Project Definition	End Usage: Typical Purpose of Estimate	Typical Budget Estimate Accuracy
Class 5	0% to 2%	Concept Screening	-30% to +50%
Class 4	1% to 15%	Study or Feasibility	-15% to +30%
Class 3	10% to 40%	Budget, Authorization, or Control	-15% to +30%
Class 2	30% to 70%	Control or Bid/Tender	-5% to +15%
Class 1	50% to 100%	Check Estimate on Bid/Tender	-5% to +15%

Table 3-1. AACE Cost Estimation Classification

**Vendor Cost Solicitation**. Technology cost information was requested from vendors for those technologies that were most promising in Phase II pilot tests (McGuire et al., 2006). This included U.S. Filter Corporation in partnership with Rohm and Haas (US Filter/R&H) weak- and strong-base ion exchange. In addition, we requested a cost quotation from BasinWater, a strong-base ion exchange vendor with a containerized treatment system. Finally, various vendors were contacted for quotes on unit processes within the RCF treatment process. Vendor-supplied cost quotations were amended using independently-developed capital costs and O&M estimates, as discussed below.

**Independent Cost Development**. Capital cost estimates were developed using the MasterFormat<sup>™</sup> framework established by the Construction Specifications Institute. MasterFormat<sup>™</sup> provides an organizational structure for performance-based construction specifications and costs.



The Malcolm Pirnie Standard Specifications Format conforms closely to the Construction Specification Institute's (CSI) MasterFormat 1995. The Malcolm Pirnie Standard Specifications Format is based on a Division-Section concept. Each Division is identified by a Division number and title. The Division Title is a broad generic heading based on an interrelationship of place, trade, function, or material. There are eighteen Divisions that are constant in sequence, name, and number, are as follows:

Division 0 -	Bidding Requirements, Contract Forms, Conditions of Contract
Division 1 -	General Requirements
Division 2 -	Site Construction
Division 3 -	Concrete
Division 4 -	Masonry
Division 5 -	Metals
Division 6 -	Wood and Plastics
Division 7 -	Thermal and Moisture Protection
Division 8 -	Doors and Windows
Division 9 -	Finishes
Division 10 -	Specialties
Division 11 -	Equipment
Division 12 -	Furnishings
Division 13 -	Special Construction
Division 14 -	Conveyance Systems
Division 15 -	Mechanical
Division 16 -	Electrical
Division 17 –	Instrumentation and Controls

The Division Titles are primarily an organizational device. Each Division contains a group of related Sections, with each Section generally constituting a unit of work or a single entity such as a particular material, product, or item of equipment.

In addition to specific estimates associated with each Division, several standard capital cost multipliers were applied to the total capital cost (Table 1).

Capital Cost	Cost Multiplier
Insurance	2.5%
Bonds	2.0%
Contractor Overhead and Profit	10%
Engineering	10%
Contingency	20%

Table 3-2. Standard Capital Cost Multipliers



**General Cost Assumptions.** A capital interest rate of 5% with a recovery period of 20 years was used to annualize all technology capital costs. All costs are expressed in September 2006 dollars. Labor costs were estimated for each technology based on full-time equivalents (FTEs) with a loaded annual salary of \$100,000 (typical estimate for Glendale, California).



### Weak Base Anion Exchange

**Treatment Process Description**. A WBA exchange system would consist of lead/lag resin vessels with upstream acid addition. Due to its high capacity and difficulty in regeneration, WBA resin is intended be used as a once-through, non-regenerable media. Figure 1 provides a process flow schematic of a WBA system.



Figure 4-1: Process Flow Schematic of US Filter/R&H WBA System

This system includes acidification of the influent to protonate the resin for optimal Cr(VI) removal and to limit OH competition with chromate ions. Acid requirements for pH depression to 6.0 determined from the Phase III Bridge Project were approximately 0.00023 gallons of 31% HCl per gallon of water treated. US Filter/R&H specified a volumetric design flow rate for this media of approximately 2.5 gpm per cubic feet, bed volumes of 200 cubic feet, and 8-ft. diameter vessels. Cost estimates are based on removal of Cr(VI) to approximately 100,000 bed volumes, which represents operation to

maximize Cr(VI) capacity but minimize the accumulation of uranium on the resin (i.e., to prevent the formation of low-level radioactive waste). This throughput corresponds to approximately 207 days of operation before the resin is replaced. US Filter/R&H estimated that a weekly low-volume backwash may be necessary to reclassify the media bed, which would yield non-hazardous backwash water.

**Capital Cost Development**. For the 500 gpm demonstration system, two 8-ft. diameter vessels would be plumbed in lead/lag configuration. The 1,000 gpm demonstration system would have two 12-ft. diameter vessels. Other equipment included in this cost estimate are bag filters, a HCl storage and handling system, and a 16,000-gallon liquid waste equalization tank, and a centrifugal pump for regulating the spent backwash water flow to the sewer. Two parallel bag filter housings (5 micron filters, 3-ft. diameter housings) were considered in the estimate. For acid feed, cost estimates were developed using metering pumps capable of 288 gallons per day, a 2,000-gallon HCl storage tank (with a 3,000-gallon secondary containment fiberglass reinforced plastic (FRP) tank), and a scrubber system for acid vapors.

The initial resin inventory (400 cubic feet – divided into two vessels) is also included in the capital cost estimate at a rate of \$500/cubic foot (i.e., the estimate provided by US Filter/R&H, which includes loading and disposal of spent resin). Additional resin loads besides the first fill are accounted for in the O&M costs. Other one-time capital costs are shown by Division in Appendix A.

**Operation and Maintenance Cost Development**. Operating costs for the WBA system were provided by US Filter/R&H and adjusted as necessary. Estimates included the following:

- Media replacement every 207 days, at \$500 per cubic foot,
- Hydrochloric acid for pH depression, at \$1.15/gallon for 2,000 gallon loads of 31% HCl (quote obtained from Basic Chemical, October 2006),
- Non-hazardous liquid waste disposal for backwash, at \$3.22 per 1,000 gallons,
- Bag filter replacement costs, assuming monthly replacement of filters,
- Effluent booster pump energy costs, and
- Labor costs for 0.125 FTE.

The US Filter/R&H WBA system costs are dominated by O&M costs comprised largely of resin costs and acid costs for pH depression. The resin replacement costs are driven by two key assumptions: (1) the anticipated resin usage rate is based on 100,000 bed volumes to breakthrough; and (2) the cost of resin estimated at \$500/cf. The cost of WBA resins has varied significantly in the past two years, increasing from \$350/cf to \$500/cf.

Since the WBA resin requires pH depression to approximately 6.0, the acid needs are significant in Glendale's groundwater that is supersaturated with CO<sub>2</sub>. Phase III Bridge Project testing indicated that the pressurized well water at GS-3 was found to have a pH of 6.8 rather than the pH of 7.2-7.3 that is routinely measured in the laboratory (from

samples that released  $CO_2$  when brought to atmospheric pressure). At a pH of 6.0, approximately 0.00023 gallons of 31% HCl will be needed, which corresponds to about 165 gallons of 31% HCl per day for a flow rate of 500 gpm. Although not tested at pilot-scale, cost savings may be realized if sulfuric acid can be used; this may be a variable that could be tested in the demonstration study.

Residuals streams from the WBA system are limited to spent resin and backwash water. Non-hazardous backwash water could be sent to either the Los Angeles sewer facilities (for the Southern wells) or to the Glendale sewer (for the Northern wells). Spent resin will be hazardous due to high chromium levels, as shown by the California WET test results in the Phases II and III projects.

**Estimated Cost Range**. Based on vendor-provided cost estimates and an independent analysis of costs, estimates were developed of the cost range for WBA systems. For WBA, a third case was considered – a 500 gpm retrofit of two GAC vessels at the GS-3 site, which was estimated to save over \$600,000 for capital costs associated with the WBA system.

Figure 2 shows the capital cost and annual O&M cost estimates for 500 and 1,000 gpm systems. Figure 3 displays the annualized costs in dollars per acre-foot of water treated.



Figure 4-2: Capital Cost Estimates and Annual O&M of the WBA System





Figure 4-3: Annualized Cost Estimates of the WBA System

As noted previously and shown in Figure 3, the O&M costs are the largest cost component of the annualized costs, which is due to both resin replacement frequency and acid needs. Since resin costs dramatically increased from 2005 estimates likely due to market pricing, the potential exists for resin costs to come down, particularly if other WBA resins are available to provide competition.

# Strong Base Anion Exchange

**Treatment Process Description**. In the past Phase II cost estimate, US Filter/R&H provided a quotation for a strong base anion exchange system. However, after obtaining experience with this process in Colby, Kansas, US Filter no longer offers regenerable SBA for Cr(VI) removal. During this testing, US Filter encountered difficulty in regenerating the resin to full capacity after approximately 12 to 15 regenerations. Consequently, US Filter now markets only the WBA system and a single-pass SBA system.

An important point about this SBA system is BasinWater's contention that the process is much more efficient than typical SBA systems. As a result, the amount of salt used in the BasinWater system will supposedly be much lower (59 lbs./AF water treated) than other brine regeneration applications (such as Calgon's ISEP process for perchlorate, which uses about 1,600 to 2,400 lbs./AF). Partial data was provided for a BasinWater chromate removal system in Stockton, California; however, no proof of effective regeneration past 12 to 15 cycles was provided.



Figure 4-4: General Process Flow Schematic of an SBA System

The BasinWater system also contains a brine processing unit to process the spent brine, thus rendering it non-hazardous. Cr(VI) is reduced and precipitated using a ferrous salt.



The solid waste component will be hazardous by California WET standards. Additional details on the brine processing unit have not been provided by BasinWater.

**Pilot testing results.** Phase II pilot testing showed that US Filter/R&H SBA Resin PWA410Cl was effective at removing Cr(VI) to less than 5  $\mu$ g/L for approximately 1,900 bed volumes. The SBA resin was effectively regenerated using a saturated brine solution recycled up to 7 times during pilot testing. The need for a lead/lag configuration or multiple beds-in-parallel was confirmed when chromatographic peaking of nitrate was observed, yielding effluent concentrations exceeding the MCL for nitrate. No specific testing on the BasinWater system was conducted; this would have to be done at the demonstration scale if the technology is selected for additional testing.

**Capital Cost Development.** Capital cost estimates provided by BasinWater include a treatment module (mobile container), 6,500-gallon salt storage (saturator) tank, two 6,500-gallon brine wastewater storage tanks, and a brine processing unit. BasinWater provided several options for their system, including purchase, a take-or-pay option with a 10-year service agreement, and a monthly standby with a water service agreement. For purposes of cost comparison, the purchase option was considered in this evaluation. Other one-time capital costs are shown by Division in Appendix A.

**Operation and Maintenance Cost Development**. Operating costs for the SBA system were provided by BasinWater and adjusted as necessary. Estimates included the following:

- Salt usage, estimated at 59 lbs. per acre-foot of water treated at \$100/ton of salt,
- Non-hazardous backwash water disposal, at \$3.22 per 1,000 gallons,
- Non-hazardous brine disposal, including trucking costs and discharge fees to Hyperion for a total cost of \$0.15/gallon,
- Solid hazardous waste disposal at a rate of \$445/ton,
- Bag filter replacement costs, assuming monthly filter replacement,
- Effluent booster pump energy costs, and
- Labor costs for 0.5 FTE.

Residuals disposal cost estimates dominated the O&M costs due to the need for trucking non-hazardous (treated) brine to a sewer connection leading to Hyperion. This step is required since the Glendale Wastewater Reclamation Plant will not accept brine. The potential for brine recycle has not been offered by BasinWater and may offer the potential for reduced spent brine volumes. The volume of non-hazardous brine includes regenerant and slow rinse liquid waste. Other sources of residuals waste include fast rinse and backwash liquid waste, which will be sent to the sewer as non-hazardous liquid waste, and solid hazardous waste from brine processing.

Estimated Cost Range. Based on vendor-provided cost estimates and an independent analysis of costs, cost estimates were prepared for SBA treatment. Figure 5 shows total

capital cost and annual O&M cost estimates for 500 and 1,000 gpm systems. Figure 6 displays the annualized costs for SBA systems in dollars per acre-foot of water treated. As shown in Figure 6, the O&M and capital costs are similar on an annualized basis.



Figure 4-5: Capital Cost Estimates of the BasinWater SBA Treatment System









Several variables associated with the SBA technology are unknowns that have the potential to significantly impact SBA treatment process feasibility, including:

- BasinWater has not released data proving the capabilities of the brine processing unit for rendering the liquid component of the brine non-hazardous. Limited research has demonstrated this brine treatment approach, and it is uncertain if the capital (e.g. dewatering equipment) and O&M (e.g. increased labor necessary to manage spent brine treatment and sludge disposal, estimated here to be an extra 0.5 FTE) estimates provided by BasinWater are accurate. Consequently, the residuals cost estimates for the brine treatment systems may not reflect all of the anticipated costs associated with this approach. At this time, however, these costs reflect information provided by BasinWater.
- The amount of salt required for BasinWater SBA regeneration is very low compared to regenerable SBA processes for perchlorate. If larger quantities are required than those estimated by BasinWater, the brine processing unit may be undersized and quantity of waste underestimated.
- Disposal of brine to a connection leading to the Hyperion sewer is not certain in the future; if this is unavailable, costs of brine disposal may significantly increase.
- No data has been provided by BasinWater assuaging the concern that SBA resins may not be regenerable beyond 12 to 15 bed volumes of water treated (as observed by US Filter).



# Reduction, Coagulation, Filtration

**Treatment Process Description**. The removal of hexavalent chromium, Cr(VI), by reduction to trivalent chromium, Cr(III), with ferrous sulfate and subsequent coagulation with ferric iron followed by filtration was demonstrated to successfully remove Cr(VI) during pilot testing. The RCF pilot unit consisted of a reduction tank, aeration columns, and dual-media granular filters; in addition, chemical feed points included those for pH control before the reduction tank and aeration columns, ferrous sulfate addition before the reduction tank, and filter aid polymer addition prior to the filters.

Since the RCF process had never been utilized to remove Cr(VI) in a potable drinking water supply, the RCF technology costs were estimated using a range of sources including quotes from vendors that could supply different unit processes. Figure 7 illustrates the RCF system process flow diagram.



### Figure 4-7: Process Flow Schematic of the RCF System

**Pilot testing results.** Pilot testing efforts identified optimal operating conditions for the RCF process. At ambient pH conditions and a Fe(II):Cr(VI) mass ratio of 25:1, the system continuously removed chromium (both Cr(VI) and Cr(III)) to below detectable levels for 48 hours before filter head loss and turbidity goals were exceeded. The pilot system was backwashed with air scour and bed fluidization. The bed expansion rate was



controlled at 20 to 30%, and the entire backwash procedure was complete within 10 to 12 minutes.

Waste minimization and disposal options for the chromium-containing backwash water solids were also investigated during pilot testing. It was determined that the backwash solids could be rapidly settled with low doses (0.2 to 1.0 mg/L) of high molecular weight polymer. The resultant settled backwash water may be suitable for recycle to the head of the system, while the settled backwash solids would be dewatered. The liquid residual from the dewatering process would be classified as non-hazardous and sent to the sewer. The dewatered solids would be classified and disposed of as hazardous solid waste.

**Capital Cost Development**. Capital costs for the RCF process include the chemical feed systems, reduction tank, settler, aeration chamber, filters, backwash pumping, and waste handling treatment equipment. Since the pilot testing identified ambient pH conditions as optimal, pH adjustment equipment has not been included in this estimate. One time capital costs developed specifically included the following:

- Reduction tank with mixers (30,000-gallon),
- Gravity settler,
- Aeration chamber (10,000-gallon, with coarse air diffusers, air compressor, and blowers),
- Dual media filter (5-cell),
- Ferrous sulfate feed system, including chemical storage and pumps,
- Polymer addition feed system,
- Backwash water storage tank (30,000-gallon),
- Backwash water (post-backwash) holding tank with mixer (20,000-gallon),
- Belt filter press (1-meter), and
- Booster pumps.

The capital costs estimated for the RCF system are higher than the other technologies evaluated, primarily due to the cost of filters and backwash waste handling and treatment equipment required to dewater the backwash solids. As a potential alternative to granular media filters, microfiltration might offer cost savings. Alternate filtration strategies could be evaluated in the demonstration-scale design.

**Operation and Maintenance Cost Development**. Operational costs for the RCF process included the following:

- Ferrous sulfate costs, at \$0.60/gallon (5% Fe) based on a usage rate mass ratio of 25:1 Fe:Cr (2.5 mg/L as Fe for 100 μg/L Cr),
- Non-hazardous backwash water disposal, at \$3.22 per 1,000 gallons,
- Solid hazardous waste disposal at a rate of \$445/ton,
- Filter media replacement, assuming 10% media loss per year,
- Effluent booster pump energy costs, and
- Labor costs for 0.5 FTE.



Residuals streams produced by the RCF process include dewatering liquids classified as non-hazardous waste and sent to sewer, as well as dewatered chromium-containing coagulation solids disposed of as hazardous solid waste. Residuals stream volumes were estimated based on full-scale operational conditions including 24-hour filter run times with a 15-minute backwash duration at 15 gpm/ft<sup>2</sup>. These conditions result in a backwash water volume of 4% of the treated flow. A number of assumptions were then needed to calculate liquid and solid residuals components. The RCF residuals disposal cost estimates rely heavily on the operational assumptions for the process, including backwash duration and quantity, settled backwash water sludge volume, and dewatering efficiency. These operational assumptions dictate the total volumes of dewatering liquids classified as non-hazardous that are sent to sewer, as well as dewatered chromium-containing coagulation solids disposed of as hazardous solid waste. With no available full-scale operational history for the RCF process, these assumptions were limited to industry experience and such texts as *Water Quality and Treatment* citing coagulation practice (Cornwell, 1999).

Of the backwash water, 0.58% was assumed to be settled sludge (based on calculations of ferrous doses), and 99.42% of the flow was assumed to be recycled to the head of the plant. The settled sludge was assumed to have 3% solids, and the filter press was assumed to have 80% dewatering efficiency (Cornwell, 1999). These assumptions led to an estimate of 28,000 gallons per day of non-hazardous backwash water sent to the sewer for a 500 gpm system – a small cost component. Solid residuals, on the other hand, were a significant cost at \$445/ton and an estimated 20 tons produced per year.

**Estimated Cost Range**. Based on vendor-provided cost estimates of unit processes and an independent analysis of costs, costs were developed for the RCF treatment process for 500 and 1,000 gpm flows. Figure 8 shows total capital cost and annual O&M cost estimates for two different size systems. Figure 9 displays the annualized costs for RCF systems in dollars per acre-foot of water treated. In general, the RCF system costs are characterized by relatively low O&M costs and high capital costs.





Figure 4-8: Capital Cost Estimates of the RCF Treatment System

**Design Capacity & Technology** 











Figure 10 shows a comparison of the capital cost estimates for each of the three technologies at 500 and 1,000 gpm. The figure highlights the relatively high capital costs associated with the RCF technology. SBA and WBA applications had similar capital costs, although the potential retrofit at GS-3 significantly reduced the capital cost by more than \$600,000.

Annual O&M cost estimates are presented in Figure 11. In general, SBA and RCF had lower O&M costs than WBA resin. The high cost of resin replacement and (secondly) acid costs in the WBA system eclipsed the residuals disposal costs that contributed much of the SBA and RCF O&M costs. Finally, Figure 12 shows an annualized cost comparison of the various technologies.



Figure 5-1: Comparison of Capital Cost Estimates for the Three Technologies at Two Flow Rates





Figure 5-2: Comparison of Annual O&M Cost Estimates for the Three Technologies at Two Flow Rates

Figure 5-3: Comparison of Annualized Cost Estimates for the Three Technologies at Two Flow Rates



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Glendale Water and Power Refined Cost Estimates for Hexavalent Chromium Removal Technologies Refined cost estimates were developed for three chromium treatment technologies (SBA, WBA, and RCF) using vendor-based estimates and standard cost estimation practices. For each technology, primary cost drivers were identified and are shown below:

- US Filter/ Rohm & Haas WBA (Duolite A7 resin): Approximately 67% of the annualized costs were O&M costs, including resin replacement and acid for pH depression. This technology is particularly advantageous as a once-through treatment system with only solid residuals (i.e. no brine). Potential exists for the resin cost to be reduced, since costs were significantly lower less than 2 years before this cost update.
- BasinWater Strong Base Anion Exchange: BasinWater system success is predicated on several key unknowns. First, the ability to regenerate the resin many times has been called into question by US Filter's refusal to sell SBA for chromate treatment due to loss of resin capacity after multiple regenerations. Second, brine processing yielding a non-hazardous liquid waste and hazardous solid waste is critical to providing the low costs shown in this evaluation. Inability to make the brine nonhazardous would render the technology significantly more expensive, as shown in the previous Phase II cost evaluation. Finally, the likelihood of future brine disposal to a sewer connection leading to Hyperion introduces a large unknown to the process. Overall, demonstration testing would be critical to ensure that this technology is able to meet performance expectations set forth by BasinWater.
- Reduction/Coagulation/Filtration: Annual costs were split between capital costs, operating costs, and residuals costs. Residuals disposal contributed the largest annual cost, followed by capital due to the need for filters and backwash handling and treatment. Other filtration strategies, such as microfiltration, may offer cost savings in the filtration capital costs. Further testing would be necessary to determine the effectiveness of alternate filtration strategies.

Overall, cost estimates developed in this project revealed that annualized costs were lowest for SBA with brine treatment (assuming non-hazardous brine could be disposed to the sewer over the long term), followed by RCF, then WBA. At 500 gpm, the WBA retrofit of existing GS-3 vessels was comparable to the RCF costs on an annualized basis.



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- OEHHA. 1999. Public Health Goal for Chromium in Drinking Water. California Environmental Protection Agency.
- Qin, G., M.J. McGuire, N.K. Blute, C. Seidel, L. Fong. 2005. Pilot Studies of Hexavalent Chromium Removal by Reduction with Ferrous Sulfate, Coagulation, and Filtration. *Environ. Sci. Technol.*, 39:16, 6321-6327.
- US Filter. 2006. Proposed Cost Information for Hexavalent Chromium Treatment. Submitted to McGuire Malcolm Pirnie. September 2006.
- US Filter. 2006. Proposed Retrofit Cost Information for Hexavalent Chromium Treatment at GS-3. Submitted to McGuire Malcolm Pirnie. March 2006.



Technology Cost Estimates, including Capital Cost Summaries, Capital Cost Details, and Operations and Maintenance Costs:

- USFilter/R&H Weak Base Anion Exchange (at pH 6.0) 500 gpm
- USFilter/R&H Weak Base Anion Exchange (at pH 6.0) 500 gpm Retrofit
- USFilter/R&H Weak Base Anion Exchange (pH 6.0) 1,000 gpm
- BasinWater Strong Base Anion Exchange 500 gpm
- BasinWater Strong Base Anion Exchange 1,000 gpm
- Reduction, Coagulation, Filtration 500 gpm
- Reduction, Coagulation, Filtration 1,000 gpm

## US Filter/R&H Weak Base Anion Exchange (pH 6.0) – 500 gpm:

	City of G Capital Cost Estimate - Weak	ilendale Base Anion (WBA) 500 gpm			
Company:	Malcolm Pirnie, Inc.	Date: 29-Sep-06			
Project:	Phase III Hexavalent Chromium Demonstration System	Estimator: SMD			
Submittal:	Conceptual Design Level Cost Estimate	Checker: GB, MJM, NKB			
Work Task:		Cost Index: ENR CCI = 8572.47 (Los Ang	geles, September 2006		
	Division Summary		Total		
	Division 1 - General Conditions		\$50,000.00		
	Division 2 - Site Construction		\$81,690.00		
	Division 3 - Concrete		\$55,500.00		
	Division 4 - Masonry		\$0.00		
	Division 5 - Metals		\$15,500.00		
	Division 6 - Wood & Plastics		\$0.00		
	Division 7 - Thermal & Moisture Protection		\$250.00		
	Division 8 - Doors & Windows		\$0.00		
	Division 9 - Finishes		\$14,750.00		
	Division 10 - Specialties		\$500.00		
	Division 11 - Equipment		\$604,059.60		
	Division 12 - Furnishings		\$0.00		
	Division 13 - Special Construction		\$21,600.00		
	Division 14 - Conveying Systems		\$0.00		
	Division 15 - Mechanical		\$34,640.00		
	Division 16 - Electrical		\$150,000.00		
	Division 17 - Instrumentation and Control		\$115,000.00		
		Division 1 - 17 Subtotal	\$1,143,489.60		
	Insurance @ 2.5%				
		Bonds @ 2.0%	\$22,869.79		
		Overhead & Profit @ 10%	\$114,348.96		
		Engineering @ 10%	\$114,348.96		
		Total	\$1,423,644.55		
	Contingency @ 20.0%				
	CONCEPTUAL LEVEL PROBABLE CONSTRUCTION COST				
		(September 2006)			



	City of Capital Cost Estimate - Wea	Glendale ık Base Anic	on (WBA) 500 g	om		
Company:	Malcolm Pirnie, Inc.		Date:	29-Sep-06		
Project:	Phase III Hexavalent Chromium Demonstration System		Estimator:	SMD		
Submittai: Work Task:	Conceptual Design level Cost Estimate		Checker: Cost Index:	GB, MJM, NKB ENR CCI = 8572.47	(Los Angeles, Se	ptember 2006)
	Specification Section	Unit	Quantity	Cost	Installation Factor	Total
Division 1 - 0 Div 1	General Conditions	LS	1	\$50,000.00	1.0	\$ 50,000.00
	Mobilization/Demobilization	+				
	Division 1 Total	+				\$50,000.00
Division 2 - 9	Site Construction		1	¢ 5,000,00	10	\$5,000,00
02220	Site Preparation Clearing	LO	1	\$ 5,000.00	1.0	τουυ,σφ
02313	Excavation and Backniii Excavation and grading of of demonstration facility limits	LS	1 570	\$ 50,000.00	1.0	\$50,000.00
	Excess Material to be removed Backfill	CY	785	\$ 0.00 \$ 18.00	1.0	\$12,500.00 \$14,130.00
	Division 2 Total					\$81,690.00
Division 3 - 0	Concrete					
03100	Concrete Formwork Concrete	-		In 03300		
	Equipment Slab (3,000-sf)	CY	111	\$ 500.00	1.0	\$55,500.00
	Division 3 Total					\$55,500.00
Division 4 - I	Nasonry					
Division 5 - I	Metals					
05051 05501	Anchor Bolts, Toggle Bolts, and Concrete Inserts Miscellaneous Metal Fabrications (includes access platforms)	LS LS	1	\$ 500.00 \$ 15,000.00	1.0 1.0	\$500.00 \$15,000.00
	Division 5 Total					\$15,500.00
Division 6 - 1	Nood & Plastics	+				
Division 7 -	Ti					
07920	Caulking and Sealants	LS	1	\$ 250.00	1.0	\$250.00
	Division 7 Total					\$250.00
Division 8 - I	Doors & Windows					
Division 9 - [	Finishes	+				
09611	Concrete Hardener	SF	3,000	\$ 3.25	1.0	\$9,750.00 \$5,000.00
09900	Painting	Lo	1	\$ 5,000.00	1.0	\$14,750,00
						\$14,700.00
Division 10 - 10400	Specialties Identification Devices	LS	1	\$ 500.00	1.0	\$500.00
	Division 10 Total					\$500.00
Division 11 -	Eauipment	+				
11179	Fiberglass Reinforced Plastic Tanks (HCl bulk Storage Tank)	LS	1	\$ 5,000.00 • 12,500.00	1.2	\$6,000.00 \$15,000.00
11216	Hydrochloric Acid Feed System w/ scrubber Bag Eilione	LS	· 1 2	\$ 60,482.00 \$ 17,500.00	1.2	\$72,578.40 \$42,000.00
11195	Fixed Bed Ion Exchange System (Weak Base Anion)	LS	1	\$ 161,903.00	1.2	\$194,283.60
11530	Pumps, General	EA	2	\$ 14,800.00	1.2	\$35,520.00
	Division 11 Total					\$604,059.60
Division 12 -	Furnishings					
Division 13 -	Special Construction	┨──┤				
13125	FRP Walk-In Enclosure (MCC)	LS	1	\$ 18,000.00	1.2	\$21,600.00
	Division 13 Total	+				\$21,600.00
Division 14 -	Conveying Systems					
Division 15 -	Mechanical					
15051	Buried Piping Installation 8" Influent Piping	FT	250	\$ 21.00	1.4	\$7,350.00
	Effluent Piping Backwash Waste Piping	FT	250 100	\$ 21.00 \$ 21.00	1.4	\$7,350.00 \$2,940.00
15052	Exposed Piping Installation Ion Exchange System Process Piping			In 11195		
15055 15061	Pipe Hangers and Supports Ductile Iron Pipe	LS	1	\$ 5,000.00 In 15051	1.0	\$5,000.00
15067 15100	Thermoplastic Pipe Valves 4-Inch and Larger	LS	1	In 15051 & 15052 \$ 10.000.00	1,2	\$12.000.00
	Division 15 Total			Ψ .=,		\$34.640.00
Division 16		1				ψ0,,
16050	General Provisions	LS	1	\$ 150,000.00	1.0	\$150,000.00
	Division 16 Total					\$150,000.00
Division 17 -	Instrumentation and Control	╂───┤				
17400	Instrumentation and Control	LS	1	\$ 115,000.00	1.0	\$ 115,000.00
	Division 17 Total					\$115,000.00
		1	1	Division	1 - 17 Subtotal	\$1.143.489.60



Glendale Water and Power Refined Cost Estimates for Hexavalent Chromium Removal Technologies

#### City of Glendale Operation and Maintenance Costs - Weak Base Anion (WBA) 500 gpm

Company:	Malcolm Pirnie, Inc.	Date:	
Project:	Phase III Hexavalent Chromium Demonstration System	Estimator:	
Submittal:	Conceptual Design Level Cost Estimate	Checker:	
Work Task:		Cost Index:	

29-Sep-06 <u>SMD</u> <u>GB, MJM, NKB</u> <u>ENR CCI = 8572.47</u> (Los Angeles, September 2006)

Item	Description	O&M Misc.	Energy	Chemicals	Waste Disposal	Total O&M	Notes
1.0	Weak Base Anion System						
1.1	Resin/Media Replacement	\$175,404				\$175,404.00	Assumed 100,000 bed-volume capacity
1.2	Pre-Filters filter replacement	\$1,440				\$1,440.00	filters Boosting IX effluent to aerator
1.3	Effluent Booster Pumps		\$6,345			\$6,344.53	influent. 500-gpm @ 50' TDH Feed water conditioning with 31% HCI. Feed Rate: 165 gpd of 31%
1.4	Chemicals			\$69,259		\$69,258.75	loads Assumed 2% of equipment costs (Div
1.5	Miscellaneous Maintenance Subtotal - WBA System	\$12,081				\$12,081.19 <b>\$264,528.48</b>	11)
2.0	Waste Disposal						
2.1 2.2	Liquid Waste Disposal (Backwash Wate Resin/Media Disposal Subtotal - Waste Disposal	er)			\$1,035	\$1,035.00 \$0.00 <b>\$1,035.00</b>	Backwash waste to sanitary sewer based on 321,000 gallons liquid waste per year (for 500-gpm system) Resin disposal costs included in resin replacement cost (if considered separately, cost would be \$1675 for 6.7 tons at \$445/ton)
3.0	Labor						
3.1	Labor Subtotal - Labor	\$12,500				\$12,500.00 <b>\$12,500.00</b>	Labor based 0.125 FTE at \$100,000/yr.
TOTAL	Subtotals Total	\$201,425	\$6,345	\$69,259	\$1,035	\$278,063.48	





## US Filter/R&H Weak Base Anion Exchange (pH 6.0) – 500 gpm Retrofit:

City Capital Cost Estimate - Weak	of Glendale Base Anion (WBA) 500 gpm Retrofit				
Company:         Malcolm Pirnie, Inc.           Project:         Phase III Hexavalent Chromium Demonstration System           Submittal:         Conceptual Design Level Cost Estimate           Work Task:	Date:         29-Sep-06           Estimator:         SMD           Checker:         GB, MJM, NKB           Cost Index:         ENR CCI = 8572.47	eles, September 2006			
Division Summary		Total			
Division 1 - General Conditions		\$25,000.00			
Division 2 - Site Construction		\$5,000.00			
Division 3 - Concrete		\$9,500.00			
Division 4 - Masonry		\$0.00			
Division 5 - Metals		\$15,500.00			
Division 6 - Wood & Plastics		\$0.00			
Division 7 - Thermal & Moisture Protection		\$0.00			
Division 8 - Doors & Windows		\$0.00			
Division 9 - Finishes		\$6,625.00			
Division 10 - Specialties		\$0.00			
Division 11 - Equipment		\$322,759.40			
Division 12 - Furnishings		\$0.00			
Division 13 - Special Construction		\$21,600.00			
Division 14 - Conveying Systems		\$0.00			
Division 15 - Mechanical		\$25,820.00			
Division 16 - Electrical		\$150,000.00			
Division 17 - Instrumentation and Control		\$115,000.00			
	Division 4 47 Outstate	\$COC 004 40			
		\$090,004.40			
	Insurance @ 2.5%	\$17,420.11			
	Durath and & Drafit @ 40%	\$13,936.09			
	Overnead & Profit @ 10%	\$69,680.44			
	Engineering @ 10%	\$05,000.44			
	Total	\$867,521.48			
	Contingency @ 20.0%				
CONCEP	TUAL LEVEL PROBABLE CONSTRUCTION COST	\$1,041,025.77			
	(September 2006)				



Company: Project: Submittal: Work Task:	mpany: Malcolm Pirnie, Inc. Project: Phase III Hexavalent Chromium Demonstration System bmittal: Conceptual Design Level Cost Estimate rk Task:			29-Sep-06 SMD GB, MJM, NKB ENR CCI = 8572.47	(Los Angeles, September 2006)		
	Specification Section	Unit	Quantity	Cost	Installation Factor	Total	
Division 1 -	General Conditions						
Div 1	General Conditions Mobilization/Demobilization	LS	1	\$ 25,000.00	1.0	\$ 25,000.00	
	Division 1 Total					\$25,000.00	
Division 2 -	Site Construction						
02220	Site Preparation	LS	1	\$ 5,000.00	1.0	\$5,000.00	
	Division 2 Total					\$5,000.00	
Division 3 -	Concrete						
03100	Concrete Formwork			In 03300			
03300	Equipment Slab (500-sf)	CY	19	\$ 500.00	1.0	\$9,500.00	
	Division 3 Total					\$9,500.00	
Division 4							
Division 4 -	Wasonry						
Division 5 -	Metals						
05051	Anchor Bolts, Toggle Bolts, and Concrete Inserts Miscellaneous Metal Fabrications (includes access platforms)	LS	1	\$ 500.00 \$ 15,000.00	1.0	\$500.00	
	Division 5 Total					\$15 500 00	
						\$10,000.00	
Division 6 -	Wood & Plastics						
Division 7 -	Thermal & Moisture Protection						
Division 8 -	Doors & Windows						
Division 9 -	l Finishes						
09611	Concrete Hardener	SF	500	\$ 3.25	1.0	\$1,625.00	
09900		1.3	, 	\$ 5,000.00	1.0	\$5,000.00	
	Division 9 Total					\$6,625.00	
Division 10 ·	Specialties						
Division 11 -	l - Equipment						
11179	Fiberglass Reinforced Plastic Tanks (HCl bulk Storage Tank)	LS	1	\$ 5,000.00	1.2	\$6,000.00	
11216	Fiberglass Reinforced Plastic Tanks (Waste Equilization Tank) Hydrochloric Acid Feed System w/ scrubber	LS LS	1	\$ 12,500.00 \$ 60,482.00	1.2 1.2	\$15,000.00 \$72,578.40	
	Fixed Bed Ion Exchange System (Weak Base Anion), includes prefilter						
11195	assistance.	LS	1	\$ 193,661.00	1.0	\$193,661.00	
11196 11530	Weak Base Anion Resin Pumps, General (Effluent Booster Pumps)	LS EA	1	\$ - \$ 14,800.00	1.0	\$0.00 \$35,520.00	
	Division 11 Total					\$222 750 40	
						\$322,739.40	
Division 12 -	· Furnishings						
Division 13 ·	- Special Construction						
13125	FRP Walk-In Enclosure (Electrical gear/MCC)	LS	1	\$ 18,000.00	1.2	\$21,600.00	
	Division 13 Total					\$21,600.00	
Division 14 -	Conveying Systems						
Division 15 ·	l · Mechanical						
15051	Buried Piping Installation	ET	100	\$ 21.00	1.4	\$2,040,00	
	Effluent Piping	FT	100	\$ 21.00 \$ 21.00	1.4	\$2,940.00	
15052	Backwash Waste Piping Exposed Piping Installation	FT	100	\$ 21.00	1.4	\$2,940.00	
16055	Ion Exchange System Process Piping	10	1	In 11195	1.0	\$5,000,00	
15055	Ductile Iron Pipe	10	1	In 15051	1.0	\$3,000.00	
15067 15100	Thermoplastic Pipe Valves, 4-Inch and Larger	LS	1	In 15051 & 15052 \$ 10.000.00	1.2	\$12.000.00	
	Division 15 Total					\$25,820,00	
						\$23,620.00	
Division 16	- Electrical	10	4	\$ 150,000,00	1.0	\$150,000,00	
10050		10		φ 130,000.00	1.0	\$150,000.00	
	Division 16 Total					\$150,000.00	
Division 17	Instrumentation and Control						
17400	Instrumentation and Control	LS	1	\$ 115,000.00	1.0	\$ 115,000.00	
	Division 17 Total					\$115,000.00	
	1			Division	1 - 17 Subtotal	\$696.804.40	

#### City of Glendale Capital Cost Estimate - Weak Base Anion (WBA) Retrofit 500 gpm Retrofit



Glendale Water and Power Refined Cost Estimates for Hexavalent Chromium Removal Technologies

#### City of Glendale Operation and Maintenance Costs - Weak Base Anion (WBA) Retrofit

Company:	Malcolm Pirnie, Inc.	Date:	29-Sep-06
Project:	Phase III Hexavalent Chromium Demonstration System	Estimator:	SMD
Submittal:	Conceptual Design Level Cost Estimate	Checker:	GB, MJM, NKB
Work Task:		Cost Index:	ENR CCI = 8572.47 (Los Angeles, September 2006)

Item	Description	O&M Misc.	Energy	Chemicals	Waste Disposal	Total O&M	Notes
1.0	Weak Base Anion System						
1.1	Resin/Media Replacement	\$175,404				\$175,404.00	Assumed 100,000 bed-volume capacity Assumed monthly replacement of bag
1.2	Pre-Filters filter replacement	\$1,440				\$1,440.00	filters Boosting IX effluent to aerator
1.3	Effluent Booster Pumps		\$6,345			\$6,344.53	influent. 500-gpm @ 50' TDH Feed water conditioning with 31% HCI. Feed Rate: 165 gpd of 31%
1.4	Chemicals			\$69,259		\$69,258.75	loads Assumed 2% of equipment costs (Div
1.5	Miscellaneous Maintenance Subtotal - WBA System	\$6,455				\$6,455.19 <b>\$258,902.47</b>	11)
2.0	Waste Disposal						
2.1	Liquid Waste Disposal (Backwash Wate	r)			\$1,035	\$1,035.00	Backwash waste based on 321,000 gallons liquid waste (for 500-gpm system) Resin disposal costs included in resin replacement cost (if considered secarately. cost would be \$1675 for
2.2	Resin/Media Disposal					\$0.00	6.7 tons at \$445/ton)
	Subtotal - Waste Disposal					\$1,035.00	
3.0	Labor						
3.1	Labor Subtotal - Labor	\$12,500				\$12,500.00 <b>\$12,500.00</b>	Labor based 0.125 FTE at \$100,000/yr.
TOTAL	Subtotals Total	\$195,799	\$6,345	\$69,259	\$1,035	\$272,437.47	



## US Filter/R&H Weak Base Anion Exchange (pH 6.0) – 1,000 gpm:

City of Gleno Capital Cost Estimate - Weak Bas	Jale e Anion (WBA) 1000 gpm					
Malcolm Pirnie, Inc.           Project:         Phase III Hexavalent Chromium Demonstration System           bmittal:         Conceptual Design Level Cost Estimate           rk Task:	Date:         29-Sep-06           Estimator:         SMD           Checker:         GB, MJM, NKB           Cost Index:         ENR CCI = 8572.47	geles, September 2006)				
Division Summary		Total				
Division 1 - General Conditions		\$75,000.00				
Division 2 - Site Construction		\$81,690.00				
Division 3 - Concrete		\$62,500.00				
Division 4 - Masonry		\$0.00				
Division 5 - Metals		\$15,500.00				
Division 6 - Wood & Plastics		\$0.00				
Division 7 - Thermal & Moisture Protection		\$0.00				
Division 8 - Doors & Windows		\$0.00				
Division 9 - Finishes		\$16,375.00				
Division 10 - Specialties		\$500.00				
Division 11 - Equipment		\$947,127.60				
Division 12 - Furnishings		\$0.00				
Division 13 - Special Construction		\$21,600.00				
Division 14 - Conveying Systems		\$0.00				
Division 15 - Mechanical		\$50,000.00				
Division 16 - Electrical		\$210,000.00				
Division 17 - Instrumentation and Control		\$165,000.00				
	Division 1 - 17 Subtotal	\$1,645,292.60				
	Insurance @ 2.5%	\$41,132.32				
	Bonds @ 2.0%	\$32,905.85				
	Overhead & Profit @ 10%	\$164,529.26				
	Engineering @ 10%					
	Total	\$2,048,389.29				
	Contingency @ 20.0%					
CONCEPTUAL	CONCEPTUAL LEVEL PROBABLE CONSTRUCTION COST					
	(September 2006)					



#### City of Glendale Capital Cost Estimate - Weak Base Anion (WBA) 1000 gpm

Company: Project: Submittal: Work Task:	1y: Malcolm Pirnie, Inc.         ct: Phase III Hexavalent Chromium Demonstration System         cal: Conceptual Design level Cost Estimate         sk:			29-Sep-06 SMD GB, MJM, NKB ENR CCI = 8572.47	(Los Angeles, September 2006)		
	Specification Section	Unit	Quantity	Cost	Installation Factor	Total	
Division 1 -	General Conditions	10	1	¢ 75.000.00	10	¢75 000 00	
DIV 1	Mobilization/Demobilization	Lõ	1	\$ 75,000.00	1.0	\$75,000.00	
	Division 1 Total					\$75,000.00	
Division 2 -	Site Construction						
02220	Site Preparation Clearing	LS	1	\$ 5,000.00	1.0	\$5,000.00	
02315	Excavation and Backfill Excavation and grading of of demonstration facility limits	LS	1	\$ 50.000.00	1.0	\$50.000.00	
	Excess Material to be removed Backfill	CY	1,570 785	\$ 8.00 \$ 18.00	1.0	\$12,560.00 \$14,130.00	
	Division 2 Total	01	100	\$ 10.00	1.0	\$14,100.00	
						\$61,030.00	
Division 3 -	Concrete Concrete Formwork			In 03300			
03300	Concrete	CY	125	\$ 500.00	10	\$62 500 00	
	Division 3 Total	0.	120	\$ 000.00		\$62,500.00	
-						\$62,500.00	
Division 4 -	Masonry						
Division 5 -	Metals		-				
05051	Anchor Bolts, Toggle Bolts, and Concrete Inserts Miscellaneous Metal Fabrications (includes access platform)	LS	1	\$ 500.00 \$ 15,000.00	1.0 1.0	\$500.00 \$15,000.00	
-	Division 5 Total					\$15,500.00	
Division 6 -	Wood & Plastics						
Division 7	 		-				
Division 7							
Division 8 -							
Division 9 - 09611	Finishes Concrete Hardener	SF	3,500	\$ 3.25	1.0	\$11,375.00	
09900	Painting	LS	1	\$ 5,000.00	1.0	\$5,000.00	
-	Division 9 Total					\$16,375.00	
Division 10	Specialties					·	
10400	Identification Devices	LS	1	\$ 500.00	1.0	\$500.00	
	Division 10 Total					\$500.00	
Division 11 -	- Equipment	19	1	\$ 5,000,00	12	\$6,000,02	
44040	Fiberglass Reinforced Plastic Tanks (Waste Equilization Tank)	LS	1	\$ 12,500.00	1.2	\$15,000.00	
11216	Bag Filters	EA	2	\$ 80,184.00 \$ 19,750.00	1.2	\$96,220.80	
11195	Fixed Bed Ion Exchange System (Weak Base Anion) Weak Base Anion Resin	LS	1	\$ 217,692.00 \$ 397,797.00	1.2 1.2	\$261,230.40 \$477,356.40	
15130	Pumps, General	EA	2	\$ 18,300.00	1.2	\$43,920.00	
	Division 11 Total					\$947,127.60	
Division 12	Furnishings						
Division 13 ·	Special Construction				1 1		
13125	FRP Walk-In Enclosure (MCC)	LS	1	\$ 18,000.00	1.2	\$21,600.00	
	Division 13 Total					\$21,600.00	
Division 14	Conveying Systems						
Division 15	l - Mechanical						
15051	Buried Piping Installation	FT	250	\$ 25.00	1.4	\$8,750,00	
	Effluent Ping Backwach Weste Dining	FT	250	\$ 25.00 \$ 25.00	1.4	\$8,750.00	
15052	Exposed Piping Installation	FI	100	\$ 23.00	1.4	\$3,500.00	
15055	Pipe Hangers and Supports	LS	1	\$ 5,000.00	1.0	\$5,000.00	
15061 15067	Ductile Iron Pipe Thermoplastic Pipe			In 15051 In 15051 & 15052			
15100	Valves & Fittings (Misc.), 4-Inch and Larger	LS	0	\$ 20,000.00	1.2	\$24,000.00	
	Division 15 Total					\$50,000.00	
Division 16 -	- Electrical	LS	1	\$ 210.000.00	1.0	\$210.000 00	
	Division 16 Total		· · · ·			\$210,000,00	
						<i>\\\</i> 210,000.00	
17400	- Instrumentation and Control	LS	1	\$ 165,000.00	1.0	\$ <u>165,000</u> .00	
	Division 17 Total					\$165,000.00	
				Division	1 - 17 Subtotal	\$1.645 292 60	
					Jubiolal	ψ1,040,202.00	



Glendale Water and Power Refined Cost Estimates for Hexavalent Chromium Removal Technologies

#### City of Glendale Operation and Maintenance Costs - Weak Base Anion (WBA) 1000 gpm

Company:	Malcolm Pirnie, Inc.	Date:
Project:	Phase III Hexavalent Chromium Demonstration System	Estimator:
Submittal:	Conceptual Design Level Cost Estimate	Checker:
Work Task:		Cost Index:

29-Sep-06 <u>SMD</u> <u>GB, MJN, NKB</u> <u>ENR CCI = 8572.47</u> (Los Angeles, September 2006)

ltem	Description	O&M Misc.	Energy	Chemicals	Waste Disposal	Total O&M	Notes
1.0	Weak Base Anion System						
1.1	Resin/Media Replacement	\$350,808				\$350,808.00	Assumed 100,000 bed-volume capacity Assumed monthly replacement of ba
1.2	Pre-Filters filter replacement	\$1,440				\$1,440.00	filters Boosting IX effluent to aerator
1.3	Effluent Booster Pumps		\$6,345			\$6,344.53	influent. 1,000-gpm @ 50' TDH Feed water conditioning with 31% HCI. Feed Rate: 165 gpd of 31%
1.4	Chemicals			\$138,518		\$138,517.50	loads Assumed 2% of equipment costs (Div
1.5	Miscellaneous Maintenance Subtotal - WBA System	\$18,943				\$18,942.55 <b>\$516,052.59</b>	11)
2.0	Waste Disposal						
2.1	Liquid Waste Disposal (Backwash Water	)			\$2,363	\$2,363.00	Backwash waste based on 733,000 gallons liquid waste (for 1,000-gpm system) Resin disposal costs included in replacement cost (if considered
2.2	Resin/Media Disposal Subtotal - Waste Disposal					\$0.00 <b>\$2,363.00</b>	separately, cost would be \$3350 for 13.4 tons at \$445/ton)
3.0	Labor						
3.1	Labor Subtotal - Labor	\$25,000				\$25,000.00 <b>\$25,000.00</b>	Labor based on 0.25 FTE at \$100,000/yr.
TOTAL	Subtotals Total	\$396,191	\$6,345	\$138,518	\$2,363	\$543,415.59	





## BasinWater Strong Base Anion Exchange – 500 gpm:

City of Gle	endale						
Capital Cost Estimate - Strong E	ase Anion (SBA) - 500 gpm						
Company: Malcolm Pirnie, Inc.	Date: 29-Sep-06						
Submittal							
Work Task:	Cost Index: ENR CCI = 8572.47 (Los And	neles. September 2006					
		Joioo, ooptombol 2000,					
Division Summary		Total					
Division 1 - General Conditions		\$50,000.00					
Division 2 - Site Construction		\$81,690.00					
Division 3 - Concrete		\$66,500.00					
Division 4 - Masonry		\$0.00					
Division 5 - Metals		\$15,500.00					
Division 6 - Wood & Plastics		\$0.00					
Division 7 - Thermal & Moisture Protection		\$250.00					
Division 8 - Doors & Windows		\$0.00					
Division 9 - Finishes		\$16,700.00					
Division 10 - Specialties		\$0.00					
Division 11 - Equipment		\$719,344.00					
Division 12 - Furnishings		\$0.00					
Division 13 - Special Construction		\$21,600.00					
Division 14 - Conveying Systems		\$0.00					
Division 15 - Mechanical		\$34,640.00					
Division 16 - Electrical		\$150,000.00					
Division 17 - Instrumentation and Control		\$120,000.00					
	Division 1 - 17 Subtotal	\$1,276,224.00					
	Insurance @ 2.5%						
	Bonds @ 2.0%						
	Overhead & Profit @ 10%	\$127,622.40					
	Engineering @ 10%	\$127,622.40					
	Total	\$1,588,898.88					
	Contingency @ 20.0%	\$317,779.78					
CONCEPTUA	L LEVEL PROBABLE CONSTRUCTION COST	\$1.906.678.66					
	(September 2006)	. ,,					





#### City of Glendale Capital Cost Estimate - Strong Base Anion (SBA) - 500 gpm

Company: Malcolm Pirnie, Inc. Project: Phase III Hexavalent Chromium Demonstration System Submittal: Conceptual Design Level Cost Estimate Work Task:			Date: Estimator Checker: Cost Index:	29-S SME GB, ENR	eep-06 MJM, NB CCI = 8572.47	(Los Angeles, September 2006)		
	Specification Section	Unit	Quantity		Cost	Installation Factor	Total	
Division 1 -	General Conditions General Conditions	LS	1	\$	50,000.00	1.0	\$ 50,000.00	
	Mobilization/Demobilization							
	Division 1 Total						\$50,000.00	
Division 2 -	Site Construction			_				
02220	Site Preparation Clearing	LS	1	\$	5,000.00	1.0	\$5,000.00	
02315	Excavation and Backfill Excavation and grading of of demonstration facility limits	LS	1	\$	50,000.00	1.0	\$50,000.00	
	Excess Material to be removed Backfill	CY CY	1,570 785	\$ \$	8.00 18.00	1.0 1.0	\$12,560.00 \$14,130.00	
	Division 2 Total						\$81,690.00	
Division 3 -	Concrete							
03100	Concrete Formwork				In 03300			
03300	Equipment Slab	CY	133	\$	500.00	1.0	\$66,500.00	
	Division 3 Total						\$66,500.00	
Division 4 -	Masonry							
Division F	Matala							
05051	Anchor Bolts, Toggle Bolts, and Concrete Inserts	LS	1	\$	500.00	1.0	\$500.00	
05501	Miscellaneous Metal Fabrications (includes access platforms)	LS	1	\$	15,000.00	1.0	\$15,000.00	
	Division 5 Total						\$15,500.00	
Division 6 -	Wood & Plastics							
Division 7 -	Thermal & Moisture Protection			_				
07920	Caulking and Sealants	LS	1	\$	250.00	1.0	\$250.00	
	Division 7 Total						\$250.00	
Division 8 -	Doors & Windows							
Division 9 -	Finishes	05	0.000	<u>^</u>	0.05	1.0	<b>*</b> 11 700.00	
09611	Painting	LS	3,600	\$ \$	3.25 5,000.00	1.0	\$11,700.00	
	Division 9 Total						\$16,700.00	
Division 10	- Specialties							
Division 11	- Environment							
11197	Strong Base Anion Equipment (BWiX Treatment System)	LS	1	\$	683,824.00	1.0	\$683,824.00	
11530	Pumps, General	EA	2	\$	14,800.00	1.2	\$35,520.00	
	Division 11 Total						\$719,344.00	
Division 12	- Furnishings							
Division 13	- Special Construction							
13125	FRP Walk-In Enclosure (for MCC/electrical gear)	LS	1	\$	18,000.00	1.2	\$21,600.00	
	Division 13 Total						\$21,600.00	
Division 14	- Conveying Systems							
Division 15	- Mechanical							
15051	8" Influent Piping	FT	250	\$	21.00	1.4	\$7,350.00	
	Effluent Piping Waste Piping	FT	250 100	\$ \$	21.00 21.00	1.4 1.4	\$7,350.00 \$2,940.00	
15052	Exposed Piping Installation Ion Exchange System Process Piping				ln 11195			
15055 15061	Pipe Hangers and Supports Ductile Iron Pipe	LS	1	\$	5,000.00 In 15051	1.0	\$5,000.00	
15067	Thermoplastic Pipe	15	1	In \$	15051 & 15052	12	\$12,000,00	
	Division 15 Total			Ľ	,		\$34.640 00	
Division 10	Electrical						+= 1,040.00	
16050 16	General Provisions	LS	1	\$	150,000.00	1.0	\$150,000.00	
	Division 16 Total			Ŀ			\$150,000.00	
Division 17	- Instrumentation and Control			F				
17400	Instrumentation and Control	LS	1	\$	115,000.00	1.0	\$120,000.00	
	Division 17 Total						\$120,000.00	
<u> </u>	·		·	<u> </u>	Division	1 - 17 Subtotal	\$1,276,224.00	



Glendale Water and Power Refined Cost Estimates for Hexavalent Chromium Removal Technologies A-12

#### City of Glendale Operation and Maintenance Costs - Strong Base Anion (SBA) - 500 gpm

Company:	Malcolm Pirnie, Inc.	Date:
Project:	Phase III Hexavalent Chromium Demonstration System	Estimator:
Submittal:	Conceptual Design Level Cost Estimate	Checker:
Work Task:		Cost Index:

29-Sep-06 SMD GB, MJM, NB ENR CCI = 8572.47 (Los Angeles, September 2006)

Item	Description	O&M Misc.	Energy	Chemicals	Waste Disposal	Total O&M	Notes
1.0	Regenerable Strong Base Anion Syst	em					
1.1	Salt Usage			\$2,379		\$2,379.03	Assumed 59-lbs per acre-foot of water at \$100/ton Assumed monthly replacement of bac
1.2	Pre-Filters filter replacement	\$1,440				\$1,440.00	filters
1.3	Effluent Booster Pumps		\$6,345			\$6,344.53	Boosting IX effluent to aerator influent. 500-gpm @ 50' TDH Assumed 2% of equipment costs (Div
1.4	Miscellaneous Maintenance Subtotal - SBA System	\$14,387				\$14,386.88 <b>\$24,550.44</b>	11)
2.0	Waste Disposal						
2.1	Backwash Waste Disposal (Non-Haz)				\$696	\$696.42	Based on backwash volume of 262,800 gallons per year disposed of at sanitary sewer. Based on 1,110-gpd disposed off site to sewer leading to Hyperion (include trucking control at \$0.15 per
2.2	Brine Waste Disposal (Haz)				\$60,225	\$60,225.00	gal.
2.3	Solids Waste Disposal Subtotal - Waste Disposal				\$2,817	\$2,816.88 <b>\$63,738.30</b>	Based on 12 drums of solid waste per year at \$445/ton.
3.0	Labor						
3.1	Labor Subtotal - Labor	\$50,000				\$50,000.00 <b>\$50,000.00</b>	Labor based on 05 FTE at \$100,000/yr.
TOTAL	Subtotals Total	\$65,827	\$6,345	\$2,379	\$63,738	\$138,288.74	





## BasinWater Strong Base Anion Exchange – 1,000 gpm:

City of C Capital Cost Estimate - Strong	Slendale Base Anion (SBA) - 1000 gpm					
Company:         Malcolm Pirnie, Inc.           Project:         Phase III Hexavalent Chromium Demonstration System           Submittal:         Conceptual Design Level Cost Estimate           Work Task:	Date:         29-Sep-06           Estimator:         SMD           Checker:         GB, MJM, NB           Cost Index:         ENR CCI = 8572.47	geles, September 2006)				
Division Summary		Total				
Division 1 - General Conditions		\$75,000.00				
Division 2 - Site Construction		\$81,690.00				
Division 3 - Concrete		\$66,500.00				
Division 4 - Masonry		\$0.00				
Division 5 - Metals		\$15,500.00				
Division 6 - Wood & Plastics		\$0.00				
Division 7 - Thermal & Moisture Protection		\$0.00				
Division 8 - Doors & Windows		\$0.00				
Division 9 - Finishes		\$16,700.00				
Division 10 - Specialties		\$0.00				
Division 11 - Equipment		\$848,702.00				
Division 12 - Furnishings		\$0.00				
Division 13 - Special Construction		\$21,600.00				
Division 14 - Conveying Systems		\$0.00				
Division 15 - Mechanical		\$50,000.00				
Division 16 - Electrical		\$210,000.00				
Division 17 - Instrumentation and Control		\$120,000.00				
	Division 1 - 17 Subtotal	\$1,505,692.00				
	Insurance @ 2.5%					
	Bonds @ 2.0%					
	Overhead & Profit @ 10%					
	Engineering @ 10%					
	Total					
	Contingency @ 20.0%					
CONCEPTU	AL LEVEL PROBABLE CONSTRUCTION COST	\$2,249,503.85				
	(September 2006)					





#### City of Glendale Capital Cost Estimate - Strong Base Anion (SBA) - 1000 gpm

Company: Project:	Malcolm Pirnie, Inc. Phase III Hexavalent Chromium Demonstration System		Date: Estimator:	29-S SMD	ep-06			
Submittal: Work Task:	Conceptual Design Level Cost Estimate		Checker: Cost Index:	GB, I ENR	MJM, NB CCI = 8572.47	(Los Angeles, S	eptemb	er 2006)
	Specification Section	Unit	Quantity		Cost	Installation	Γ	Total
Division 1 -	General Conditions					1 46101		
Div 1	General Conditions Mobilization/Demobilization	LS	1	\$	75,000.00	1.0	\$	75,000.00
	Division 1 Total							\$75,000,00
								\$75,000.00
Division 2 -	Site Construction Site Preparation	LS	1	\$	5,000.00	1.0		\$5,000.00
02230	Clearing							
02010	Excavation and grading of of demonstration facility limits	LS	1	\$	50,000.00	1.0		\$50,000.00
	Backfill	CY	785	э \$	8.00	1.0		\$12,560.00 \$14,130.00
	Division 2 Total							\$81,690.00
Division 3 -	Concrete							
03100	Concrete Formwork				In 03300			
03300	Concrete Equipment Slab	CY	133	\$	500.00	1.0		\$66,500.00
	Division 3 Total							\$66,500,00
								\$00,000.00
Division 4 -	Masonry							
Division 5 -	Metals	10		¢	500.00	1.0		<b>\$</b> 500.00
05051	Miscellaneous Metal Fabrications (includes access platforms)	LS	1	ծ \$	15,000.00	1.0		\$500.00
	Division 5 Total							\$15,500.00
Division 6 -	Wood & Plactice							
Division 0 -								
Division 7 -	Thermal & Moisture Protection							
Division 8 -	Doors & Windows							
Division 9 -	Finishes				0.05	1.0		<b>A</b> 44 <b>T</b> 00 00
09611	Concrete Hardener Painting	SF LS	3,600	\$ \$	3.25 5,000.00	1.0 1.0		\$11,700.00 \$5,000.00
	Division 9 Total							\$16 700 00
Division 10	Shocialting							<i><b></b><i></i><b></b></i>
DIVISION TO								
Division 11 - 11197	- Equipment	18	1	\$	804 782 00	1.0		\$804 782 00
11530	Pumps, General	EA	2	\$	18,300.00	1.2		\$43,920.00
	Division 11 Total							\$848,702.00
Division 12 ·	l - Furnishings							
Division 13	- Special Construction							
13125	FRP Walk-In Enclosure (for MCC/electrical gear)	LS	1	\$	18,000.00	1.2		\$21,600.00
	Division 13 Total							\$21,600.00
Division 14 ·	· Conveying Systems							
Division 15	- Mechanical							
15051	Buried Piping Installation		050	¢	05.00			<b>*</b> 0 750 00
	Effluent Piping	FI	250	ъ \$	25.00	1.4		\$8,750.00
15052	Brine Waste Piping Exposed Piping Installation	FT	100	\$	25.00	1.4		\$3,500.00
15055	Ion Exchange System Process Piping Pipe Hangers and Supports	1.5	1	\$	In 11195 5 000 00	1.0		\$5,000,00
15061	Ductile Iron Pipe			Ψ In (	In 15051	1.0		\$0,000.00
15100	Valves, 4-Inch and Larger	LS	1	\$	20,000.00	1.2		\$24,000.00
	Division 15 Total							\$50,000.00
Division 16	Electrical							
16050	General Provisions	LS	1	\$	210,000.00	1.0		\$210,000.00
	Division 16 Total						1	\$210,000.00
Division 17	Instrumentation and Control							
17400	Instrumentation and Control	LS	1	\$	165,000.00	1.0		\$120,000.00
	Division 17 Total			<u> </u>			1	\$120,000.00
	•	-		•	Division 1	- 17 Subtota	I \$	1,505,692.00



Glendale Water and Power Refined Cost Estimates for Hexavalent Chromium Removal Technologies A-15

#### City of Glendale Operation and Maintenance Costs - Strong Base Anion (SBA) - 1000 gpm

Malcolm Pirnie, Inc.	Date:
Phase III Hexavalent Chromium Demonstration System	Estimator:
Conceptual Design Level Cost Estimate	Checker:
	Cost Index:
	Malcolm Pirnie, Inc. Phase III Hexavalent Chromium Demonstration System Conceptual Design Level Cost Estimate

29-Sep-06 <u>SMD</u> <u>GB, MJM, NB</u> <u>ENR CCI = 8572.47</u> (Los Angeles, September 2006)

Item	Description	O&M Misc.	Energy	Chemicals	Waste Disposal	Total O&M	Notes
1.0	Regenerable Strong Base Anion System	m					
1.1	Salt Usage			\$4,758		\$4,758.06	Assumed 59-lbs per acre-foot of water at \$100/ton Assumed monthly replacement of bag
1.2	Pre-Filters filter replacement	\$1,440				\$1,440.00	filters
1.3	Effluent Booster Pumps		\$6,345			\$6,344.53	Boosting IX effluent to aerator influent. 1,000-gpm @ 50' TDH Assumed 2% of equipment costs (Div
1.4	Miscellaneous Maintenance	\$16,974				\$16,974.04	11)
	Subtotal - SBA System					\$29,516.63	
<b>2.0</b> 2.1	Waste Disposal Backwash Waste Disposal (Non-Haz)				\$1,393	\$1,392.84	Based on backwash volume of 525,600 gallons per year disposed of at sanitary sewer.
2.2	Brine Waste Disposal (Haz)				\$120,450	\$120,450.00	(includes trucking costs) at \$0.15 per gal. Based on 24 drums of solid waste per
2.3	Solids Waste Disposal				\$5,634	\$5,633.75	year at \$445/ton.
3.0	Labor					\$1,552.04	
3.1	Labor Subtotal - Labor	\$50,000				\$50,000.00 <b>\$50,000.00</b>	Labor based on 0.5 FTE at \$100,000/yr.
TOTAL	Subtotals Total	\$68,414	\$6,345	\$4,758	\$127,477	\$206,993.23	





## Reduction, Coagulation, Filtration – 500 gpm:

City of Glendale Capital Cost Estimate - Reduction, Coagulation, Filtration (RCF) - 500 gp	m					
Company: Malcolm Pirnie Inc. Date: 29-Ser	<u>)-06</u>					
Project: Phase III Hexavalent Chromium Demonstration System Estimator: SMD						
Submittal: Conceptual Design Level Cost Estimate Checker: GB, M.	JM, NB					
Work Task: Cost Index: ENR C	CI = 8572.47 (Los Ange	eles, September 2006)				
Division Ourseau		T-1-1				
Division 1 - Conditions		10(a) \$50,000,00				
Division 2 - Site Construction		\$30,000.00				
Division 2 - Site Constituction		\$61,090.00				
Division 5 - Concrete		\$92,500.00				
Division 4 - Masonry		\$0.00				
Division 5 - Metals		\$500.00				
Division 6 - Wood & Plastics		\$0.00				
Division 7 - Thermal & Monsture Protection		\$0.00				
Division 6 - Doors & Windows		\$0.00				
Division 9 - Finishes		\$21,250.00				
Division 10 - Specialities		\$500.00				
Division 11 - Equipment		\$1,337,400.00				
Division 12 - Furnishings		\$0.00				
Division 13 - Special Construction		\$21,600.00				
Division 14 - Conveying Systems		\$0.00				
Division 15 - Mechanical		\$39,640.00				
Division 16 - Electrical		\$150,000.00				
Division 17 - Instrumentation and Control		\$115,000.00				
Divis	ion 1 - 17 Subtotal	\$1 910 080 00				
	Insurance @ 2.5%	\$47 752 00				
	Bonds @ 2.0%	\$38 201 60				
Overbe	ad & Profit @ 10%	\$101.008.00				
E	ngineering @ 10%	\$191,008.00				
	Total	\$131,000.00				
	finananan @ 00.00(	\$2,376,049.00				
	ungency @ 20.0%	\$475,609.92				
		¢2 952 650 52				
CONCEPTUAL LEVEL PROBABLE CONS						
	(Soptombor 2006)	+-,,				





### City of Glendale Capital Cost Estimate - Reduction, Coagulation, Filtration (RCF) - 500 gpm

Company:	Malcolm Pirnie, Inc.		Date:	29-Sep-06	-		
Project: Submittal:	Phase III Hexavalent Chromium Demonstration System Conceptual Design Level Cost Estimate		Estimator: Checker:	GB. MJM. NB	-		
Work Task:		Cost Index:	ENR CCI = 8572.47	(Los Angeles, Se	os Angeles, September 2006)		
				-	Installation		
	Specification Section	Unit	Quantity	Cost	Factor	Total	
Division 1 -	General Conditions	10		£ 50,000,00	10	650.000.00	
DIV 1	Mobilization/Demobilization	LS	1	\$ 50,000.00	1.0	\$50,000.00	
	Division 1 Total					\$50,000.00	
Division 2 -	Site Construction						
02220	Site Preparation	LS	1	\$ 5,000.00	1.0	\$5,000.00	
02230	Clearing Excavation and Backfill	-					
02010	Excavation and grading of of demonstration facility limits	LS	1	\$ 50,000.00	1.0	\$50,000.00	
	Excess Material to be removed Backfill	CY	1,570	\$ 8.00 \$ 18.00	1.0	\$12,560.00 \$14 130 00	
	Bookin		100	÷ 10.00	1.0	\$11,100.00	
	Division 2 Total	-				\$81,690.00	
Division 3 -	Concrete						
03100	Concrete Formwork			In 03300			
03300	Concrete Equipment Slab (5.000-sf)	CY	185	\$ 500.00	1.0	\$92,500.00	
	Division 3 Total	-				\$92,500.00	
Division 4 -	Masonry						
		1					
Division 5 -	Metals	10	1	£ 500.00	1.0	\$500.00	
05051	Anchor Boits, Toggle Boits, and Concrete Inserts	LO		\$ 500.00	1.0	\$500.00	
	Division 5 Total					\$500.00	
Division 6 -	Wood & Plastics						
Division e							
Division 7 -	Thermal & Moisture Protection						
Division 9	Deere & Windows	-					
Division 8 -		-					
Division 9 -	Finishes						
09611	Concrete Hardener	SF	5,000	\$ 3.25	1.0	\$16,250.00	
09900	Painting	LS	1	\$ 5,000.00	1.0	\$5,000.00	
	Division 9 Total					\$21,250.00	
Division 10	- Specialties	-					
10400	Identification Devices	LS	1	\$ 500.00	1.0	\$500.00	
	Division 40 Total					\$E00.00	
						\$500.00	
Division 11	- Equipment						
11179	Fiberglass Reinforced Plastic Tanks (Ferrous Sulfate Bulk Storage)	LS	1	\$ 5,000.00	1.2	\$6,000.00	
11218	Ferrous Sulfate Feed System	LS	1	\$ 30,000.00	1.2	\$36,000.00	
11219	Polymer Addition System	LS	1	\$ 20,000.00	1.2	\$24,000.00	
11216	Dual Media Filter (5-cell)	EA	1	\$ 82,900.00 \$ 450.000.00	1.2	\$99,480.00 \$540.000.00	
11311	Reduction Tank (30,000-gal. Steel Tank) w/ mixers	LS	1	\$ 70,000.00	1.2	\$84,000.00	
11312	Steel Tank (10.000-gallons)	LS	1	\$ 65,000.00	1.2	\$78,000.00	
	Blowers						
	Coarse Air Diffusers	_					
11315	Belt Filter Press (1-meter)	EA	1	\$ 220,000.00	1.2	\$264,000.00	
15120	Backwash Water Storage Tank (30,000-gal.)	LS	1	\$ 45,000.00 \$ 15,000.00	1.2	\$54,000.00	
13130	rumps, booster	LA	0	\$ 15,000.00	1.2	\$108,000.00	
	Division 11 Total					\$1,337,400.00	
Division 12	- Furnishings						
	· ····································						
Division 13	- Special Construction	1.0		• • • • • • • • •	1.0		
13125	FRP Walk-In Enclosure	LS	1	\$ 18,000.00	1.2	\$21,600.00	
	Division 13 Total					\$21,600.00	
Division 14	Convoying Systems						
DIVISION 14							
Division 15	- Mechanical						
15051	Buried Piping Installation		250	£ 21.00	1.4	67 250 00	
	Effluent Piping	FT	250	\$ 21.00	1.4	\$7,350.00	
15050	Backwash Waste Piping	FT	100	\$ 21.00	1.4	\$2,940.00	
15052	12" Influent Piping	FT		\$ 20.00	1.4	\$0.00	
15055	Pipe Hangers and Supports	LS	1	\$ 10,000.00	1.0	\$10,000.00	
15061	Thermoplastic Pipe	+		In 15051 In 15051 & 15052			
15100	Valves & Fittings (Misc.), 4-Inch and Larger	LS	0	\$ 10,000.00	1.2	\$12,000.00	
	Division 15 Total					\$39 640 00	
						<del>400,040</del> .00	
Division 16	Electrical						
16050	General Provisions	LS	1	\$ 150,000.00	1.0	\$150,000.00	
	Division 16 Total					\$150,000.00	
Division 47	Instrumentation and Control	+			<u>                                     </u>		
17400 17400	Instrumentation and Control	LS	1	\$ 115.000.00	1.0	\$115.000.00	
		1		.,			
	Division 17 Total	+			ł – – ł	\$115,000.00	
				Division	1 - 17 Subtotal	\$1,910,080.00	
		-			-		



Glendale Water and Power Refined Cost Estimates for Hexavalent Chromium Removal Technologies

## City of Glendale Operation and Maintenance Costs - Reduction, Coagulation, Filtration (RCF) - 500 gpm

Project: Phase III Hexavalent Chromium Demonstration System Estim	nator
Submittal: Conceptual Design Level Cost Estimate Che	cker:
Work Task: Cost In	ndex:

29-Sep-06 <u>SMD</u> <u>GB, MJM, NB</u> <u>ENR CCI = 8572.47</u> (Los Angeles, September 2006)

Item	Description	&M Misc	Energy	Chemicals	Waste Disposal	Total O&M	Notes
1.0	Reduction Coagulation Filtration						
1.1	Media Replacement	\$10,000				\$10,000.00	Assumed 10% media loss per year.
							Booster pumps, backwash pumps and aeration
1.2	Booster/Backwash Pumps/Blowers		\$35,928			\$35,927.83	blowers.
							Assuming a 25:1 Fe:Cr mass ratio, Fe dose of 2.5
							mg/L as Fe, and cost of 5% (as Fe) ferrous sulfate a
1.3	Chemicals			\$7,884		\$7,884.00	\$0.60/gallon
1.4	Miscellaneous Maintenance	\$26,748				\$26,748.00	Assumed 2% of equipment costs (Div 11)
	Subtotal - RCF System	1				\$80,559.83	
2.0	waste Disposal						
							Backwash water volume of 4% of water treated; 0.58% of backwash water on acttled aludge. 00.42%
							recycled: 3% solids in settled sludge: 80% filter
							press dewatering efficiency: total backwash water to
							sewer (in Glendale) of 28,000 gpd waste (for 500-
							gpm system). If no backwash water could be
							recycled, this annual sewer disposal cost would be
2.1	Liquid Waste Disposal (Non-Hazardous)				\$781	\$781.00	\$19,534 in Glendale and \$33,895 in LA
							Residuals disposal based on 20 tons/year at
2.2	Residuals Disposal (Hazardous)				\$22,695	\$22,695.00	\$445/ton
	Subtotal - Waste Disposal					\$781.00	
3.0	Labor						
3.1	Labor	\$50,000				\$50,000.00	Labor based on 0.5 FTE at \$100,000/yr.
	Subtotal - Labor					\$50,000.00	
TOTAL	Cultural	COC 740	£05.000	<b>C7</b> 00 4	¢00.470		
TOTAL	Subtotals	<b>φσ0,748</b>	<b>\$35,928</b>	۵۲,884	<b>⊅∠3,47</b> 6	\$154 025 92	
	1014					a 1.34,033,03	





## Reduction, Coagulation, Filtration – 1,000 gpm:

City of Gle Capital Cost Estimate - Reduction, Coag	ndale julation, Filtration (RCF) - 1000 gpm						
Company: Malcolm Pirnie, Inc.	Date: 29-Sep-06						
Project: Phase III Hexavalent Chromium Demonstration System	Estimator: SMD						
Submittal: Conceptual Design Level Cost Estimate	Cost Index: ENP. CCL = 8572.47 (Los And	alos Sontombor 2006)					
		eles, September 2000,					
Division Summary		Total					
Division 1 - General Conditions		\$75,000.00					
Division 2 - Site Construction		\$81,690.00					
Division 3 - Concrete		\$111,000.00					
Division 4 - Masonry		\$0.00					
Division 5 - Metals		\$500.00					
Division 6 - Wood & Plastics		\$0.00					
Division 7 - Thermal & Moisture Protection		\$0.00					
Division 8 - Doors & Windows		\$0.00					
Division 9 - Finishes		\$24,500.00					
Division 10 - Specialties		\$500.00					
Division 11 - Equipment		\$1,654,560.00					
Division 12 - Furnishings		\$0.00					
Division 13 - Special Construction		\$21,600.00					
Division 14 - Conveying Systems		\$0.00					
Division 15 - Mechanical		\$55,000.00					
Division 16 - Electrical		\$210,000.00					
Division 17 - Instrumentation and Control		\$130,000.00					
	Division 1 - 17 Subtotal						
	Insurance @ 2.5%						
	Bonds @ 2.0%	\$47,287.00					
	Overhead & Profit @ 10%	\$236,435.00					
	Engineering @ 10%	\$236,435.00					
	Total	\$2,943,615.75					
	Contingency @ 20.0%	\$588,723.15					
CONCEPTUA	L LEVEL PROBABLE CONSTRUCTION COST	\$3,532,338.90					
	(September 2006)						





#### City of Glendale Capital Cost Estimate - Reduction, Coagulation, Filtration (RCF) - 1000 gpm

Company:	Malcolm Pirnie, Inc.	Date:	29-Sep-06	-		
Submittal:	Conceptual Design Level Cost Estimate	Checker:	GB, MJM, NB	-		
Work Task:			Cost Index:	ENR CCI = 8572.47	Los Angeles, Se	ptember 2006)
	Specification Section	Unit	Quantity	Cost	Installation	Total
Division 1 -	General Conditions	0	quantity	0001	Factor	rota
Division 1 = 1	General Conditions	LS	1	\$ 75,000.00	1.0	\$75,000.00
	Mobilization/Demobilization	_				
	Division 1 Total					\$75,000.00
Division 2	Rite Construction	_				
02220	Site Preparation	LS	1	\$ 5,000.00	1.0	\$5,000.00
02230	Clearing					
02010	Excavation and grading of of demonstration facility limits	LS	1	\$ 50,000.00	1.0	\$50,000.00
	Excess Material to be removed Backfill	CY	1,570 785	\$ 8.00 \$ 18.00	1.0	\$12,560.00 \$14,130.00
	Division 2 Total					\$91 600 00
						\$81,090.00
Division 3 -	Concrete	_		L- 00000		
03100	Concrete			In 03300		
	Equipment Slab (3,500-sf)	CY	222	\$ 500.00	1.0	\$111,000.00
	Division 3 Total					\$111,000.00
Division 4 -	Masonry	-				
Division 4						
Division 5 -	Metals	18	1	\$ 500.00	10	\$500.00
03031	Anchor Boils, roggie Boils, and Concrete insens	13	-	\$ 300.00	1.0	\$500.00
	Division 5 Total					\$500.00
Division 6 -	Wood & Plastics					
Division 7	Thermal & Meisture Protection	_				
DIVISION 7 -						
Division 8 -	Doors & Windows					
Division 9 -	Finishes					
09611	Concrete Hardener	SF	6,000	\$ 3.25	1.0	\$19,500.00
09900	Painting	LS	1	\$ 5,000.00	1.0	\$5,000.00
	Division 9 Total					\$24,500.00
Division 10	- Specialties					
10400	Identification Devices	LS	1	\$ 500.00	1.0	\$500.00
	Division 10 Total					\$500.00
Division 11	- Equipment	-				
11179	Fiberglass Reinforced Plastic Tanks (Ferrous Sulfate Bulk Storage)	LS	1	\$ 5,000.00	1.2	\$6,000.00
11180	Backwash Water Holding Tank with mixer (20,000-gal.) Ferrous Sulfate Feed System	LS	1	\$ 36,600.00 \$ 34,500.00	1.2	\$43,920.00 \$41,400.00
11216	Gravity Settler	EA	1	\$ 82,900.00	1.2	\$99,480.00
11217	Polymer Addition System	LA	1	\$ 20,000.00	1.2	\$24,000.00
11311	Reduction Tank (60,000-gal. Steel Tank) w/ mixers	LS	1	\$ 110,000.00 \$ 90,000.00	1.2	\$132,000.00
	Steel Tank (10,000-gallons)					• • • • •
	Coarse Air Diffusers					
11315	Air Compressor Belt Filter Press (1-meter)	FA	1	\$ 220,000,00	12	\$264,000,00
	Backwash Water Storage Tank (30,000-gal.)	LS	1	\$ 45,000.00	1.2	\$54,000.00
15130	Pumps, Booster	EA	6	\$ 18,300.00	1.2	\$131,760.00
	Division 11 Total	_				\$1,654,560.00
Division 12	- Furnishings					
Division 12	Special Construction	_				
13125	FRP Walk-In Enclosure (MCC)	LS	1	\$ 18,000.00	1.2	\$21,600.00
	Division 13 Total	_				\$21,600,00
						\$21,000.00
Division 14 -	- Conveying Systems					
Division 15	- Mechanical					
15051	Buried Piping Installation	57	250	¢ 25.00	14	\$9.750.00
	Effluent Piping	FT	250	\$ 25.00	1.4	\$8,750.00
15052	Backwash Waste Piping Exposed Piping Installation	FT	100	\$ 25.00	1.4	\$3,500.00
15055	12" Influent Piping	FT		\$ 21.00	1.4	\$0.00
15055	Ductile Iron Pipe	10	1	In 15051	1.0	\$10,000.00
15067	Thermoplastic Pipe Valves & Fittings (Misc.), 4-Inch and Larger	LS	0	In 15051 & 15052 \$ 20.000.00	1.2	\$24.000.00
.0.00	Duision 45 Taial					¢= 1,000.00
						\$55,000.00
Division 16	- Electrical			e 010 000 ***	10	6010 000 °C
16050		LS	1		1.0	\$210,000.00
	Division 16 Total					\$210,000.00
Division 17	Instrumentation and Control					
17400	Instrumentation and Control	LS	1	\$ 130,000.00	1.0	\$130,000.00
	Division 17 Total					\$130,000.00
	1	1		Division	1 - 17 Subtotal	\$2,364.350.00



Glendale Water and Power Refined Cost Estimates for Hexavalent Chromium Removal Technologies

#### City of Glendale Operation and Maintenance Costs - Reduction, Coagulation, Filtration (RCF) - 1000 gpm

Company:	Malcolm Pirnie, Inc.	Date:
Project:	Phase III Hexavalent Chromium Demonstration System	Estimator:
Submittal:	Conceptual Design Level Cost Estimate	Checker:
Work Task:		Cost Index:

29-Sep-06 <u>SMD</u> <u>GB, MJM, NB</u> <u>ENR CCI = 8572.47</u> (Los Angeles, September 2006)

Item	Description	O&M Misc.	Energy	Chemicals	Waste Disposal	Total O&M	Notes
1.0	Reduction Coagulation Filtration						
1.1	Media Replacement	\$10,000				\$10,000.00	Assumed 10% media loss per year. Booster pumps, backwash pumps and aeration
1.2	Booster/Backwash Pumps/Blowers		\$35,928			\$35,927.83	blowers.
13	Chemicals			\$15 768		\$15,768,00	Assuming a 25:1 Fe:Cr mass ratio, Fe dose of 2.5 mg/L as Fe, and cost of 5% (as Fe) ferrous sulfate at \$0.60/gallon : Polymer addition at 1 mg/L at \$
1.4	Miscellaneous Maintenance	\$33.001		<i><b>Q</b>10,100</i>		\$33,091,20	Assumed 2% of equipment costs (Div 11)
1.4	Subtotal - RCF System	φ00,001				\$94,787.03	
2.0	Waste Disposal						
24	Listi Mart Dissert Ales Herritari				\$0.740	60.740.00	Backwash water volume of 4% of water treated; 0.55% of backwash water as settled sludge; 99.42% recycled; 3% solids in settled sludge; 80% filter press dewatering efficiency; total backwash water to sewer in Glendale of 57,600 gpd waste (for 1,000-gpm system). If no backwash water could be recycled, this annual sewer disposal cost
2.1	Liquid Waste Disposal (Non-Hazardous)				\$2,712	\$2,712.00	would be \$39,069 in Glendale and \$67,789 in LA Residuals disposal based on 40 tons/year at
2.2	Residuals Disposal (Hazardous)				\$45,390	\$45,390.00	\$445/ton
	Subtotal - Waste Disposal					\$2,712.00	
3.0	Labor						
3.1	Labor Subtotal - Labor	\$50,000				\$50,000.00 <b>\$50,000.00</b>	Labor based on 0.5 FTE at \$100,000/yr.
TOTAL	Subtotals Total	\$93,091	\$35,928	\$15,768	\$48,102	\$192,889.03	



